# Compression of Mercury at High Pressure* $\dagger$ 

Lance A. Davis and Robert B. Gordon<br>Dcpartment of Engincoring and Applicd Science, Yale University, New Haven, Connecticut

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An exact method of computing volume changes under high pressure from acoustic-wave-velocity measurcments is developed. It is applicable to large as well as small compressions. To illustrate the application of the method, precision ultrasonic-velocity measurements made in mercury at pressures up to 13 kbar for three temperatures have been used to compute $V$ as a function of $T$ and $P$. The volume is determined to an accuracy of better than $0.01 \%$ at each pressure and temperature. An analytical expression for the pressure dependence of the volume in which all coefficients are expressed in terms of the bulk modulus and its derivatives is developed and shown to give a better representation of the $P-V$ data than many of the equations now in use.

## INTRODUCTION

AFUNDANENTMI problem in high-pressure rescarch is the determination of the equation of state of condensed materials. One experimental approach to this problem is direct measurement of the volume as a function of pressure. Various methods have been devised for this. For liquids Bridgman has used a piezometer, ${ }^{1,2}$ a piston-displacement method, ${ }^{3,-5}$ and a sylphon-bellows device ${ }^{6-9}$ which employs a potentiometric length-measuring technique. The piezometer yielded volumes accurate to about $0.1 \%$, the pistondisplacement method to about $1 \%$, and the sylphon bellows to a few hundredths of $1 \%$. For solids Bridgman used a linear-compression technique ${ }^{10,11}$ where the change in length of samples relative to that of pure iron is measured and, again, the piston-displacement method. ${ }^{12-16}$ These methods have been refined by other investigators. Cutler el al. ${ }^{17}$ and Boelhouwer ${ }^{18}$ modified the sylphon-bellows technique by employing an external linear-differential transformer to measure the bellows motion. Doolittle et al. ${ }^{19}$ determined the change in volume of a liquid by following the motion of a float

[^0]at its surface with an external linear-differential transformer. Accuracies of the order of $0.01 \%$ are attained. To measure compression in solids to very high pressures, a Debye-Scherrer $x$-ray powder pattern of a sample compressed in an anvil device has been used. A review of the earlier $x$-ray techniques is given by Jamieson and Lawson ${ }^{20}$; newer methods are described by Barnett and Hall ${ }^{21}$ and Perez-Albuerne, Forsgren, and Drickamer. ${ }^{22}$ A common problem in the x -ray methods is that pressure determination is difficult so that the volume results obtained are accurate to only about $1 \%$. For compression measurements to ultrahigh pressure (megabars), the shock-wave method is used. Deal ${ }^{23}$ has given a review of the techniques involved. The question of accuracy is a difficult one here, but it is certainly not better than $1 \%$ of the volume.

In all of the experimental methods enumerated above, volume is measured directly as a function of pressure. An alternative approach, inherently capable of yielding higher accuracy, is to measure the pressure dependence of the compressibility and then obtain volume as a function of pressure by integration. The compressibility and its pressure dependence may be measured to high accuracy by acoustic methods. In 1949 Lazarus $^{24}$ initiated development of the techniques necessary for making sonic-velocity measurements to high pressure. In his work on the elastic constants of cubic single crystals he assumed the samples changed length as though they had constant compressibility. In 1957 Cook ${ }^{25}$ described a method of obtaining accurate volume results from high-pressure sonic-velocity data. He employed the less restrictive assumption that the ratio of the isothermal and adiabatic compressibilities is a constant. This approximation is reliable when the com-

[^1]pression is small, perhaps less than $1 \%$, which can of course correspond to quite high pressures for very incompressible materials. Since the velocity of sound in a material can be determined to an accuracy of $0.1 \%$ or better and this uncertainty enters the volume calculations as a relatively small additive term, volume results to better than $0.01 \%$ may be obtained. A significant advantage of this method is that it yields elastic constants and compression results simultaneously.

A disadvantage of Cook's approach is the restriction to small compressions. In this paper we develop a method which will allow the determination of accurate volume data at high pressure from elastic wave-velocity experiments regardless of the amount of compression involved. To use this method, sonic-velocity data as a function of both pressure and temperature are required; and the temperature dependence of the thermal expansion, heat capacity, and density at room pressure must be known. To illustrate the application of the method, precision sound-velocity measurements have been made in mercury over a range of temperature and pressures and used, in conjunction with available thermodynamic data, in a precision determination of volume as a function of pressure and temperature.

## EXPERIMENTAL APPARATUS AND PROCEDURE

The velocity of sound in liquid Hg is determined as a function of pressure and temperature by a variant of the pulse-echo technique originally developed by Pellam and Galt. ${ }^{26}$ The liquid Hg is placed in a stainlesssteel sample holder, and the holder placed in a cylindrical pressure vessel. Pressure is generated by driving a piston into the vessel and is transmitted to the Hg by a liquid pressure-transmission medium. Electrical leads are brought into the vessel through the base-plug pressure closure. The pressure in the vessel is determined by monitoring the resistance of a coil of Au$2.1 \% \mathrm{Cr}$ wire, which is calibrated as function of pressure vs a free-piston gauge. Experiments on the variation of sonic velocity in Hg with pressure were performed at three temperatures; $21.9^{\circ}, 40.5^{\circ}$, and $52.9^{\circ} \mathrm{C}$.

A pulsed oscillator, balancing network, preamplifier, and amplifier obtained from the Arenberg Ultrasonic Laboratory, Inc. are arranged as shown in Fig. 1. A $5-\mathrm{Mc} /$ sec pulse of $10-\mu \mathrm{sec}$ duration at a $60-\mathrm{cps}$ repetition frequency is used, and the pulse and sample echoes are displayed on a Tektronix 547 cathode-ray oscilloscope (CRO). It is somewhat difficult to make highly accurate, absolute wave-velocity measurements by the simple pulse-echo technique since it is difficult to account for the relative phase shift between echoes. Therefore, in this work the change in transit time relative to the transit time at 1 atm is measured using

[^2]

Fig. 1. The high-frequency-pulse equipment.
the first echo only. The initial transit time is computed from the 1 -atm sonic-velocity data for liquid Hg of Hubbard and Loomis ${ }^{27}$ (accurate to $0.02 \%$ ) and the known length of the sample. Correction for the change in sample length due to $T$ and $P$ was made using the measured linear-expansion coefficient for the Type 303 stainless steel used for the sample holder ${ }^{28}[16.2 \times$ $\left.10^{-6}\left({ }^{\circ} \mathrm{C}\right)^{-1}\right]$ and Bridgman's linear-compression data for $\mathrm{Fe} \mathrm{e}^{11}\left[-\Delta l / l_{0}=1.904 \times 10^{-7} P-0.22 \times 10^{-12} P^{2}\right.$ (for $P$ in bars) ]. Since the magnitude of the length change is small, high accuracy is not needed in making these corrections.
The change in transit time was determined using a variable- Hg delay line consisting of a pot of Hg with a quartz transducer at its bottom and a stecl reflector inserted into it from the top. The reflector is connected to a micrometer screw so that changes in its position can be accurately determined. At the outset of each particular high-pressure experiment, a convenient cycle of the unrectified first echo from the specimen and from the delay line is placed in phase on the CRO by adjusting the level of the reflector in the delay line. With the unrectified signals the cycles can be matched to within $\pm 1.4 \mathrm{nsec}$. With application of pressure to the sample a change in transit time results causing a shift in position of the sample echo on the CRO. By adjusting the reflector height in the delay line the same cycles were again brought into coincidence. The change in transit time is then given by $\Delta t=2 \Delta d / c$, where $\Delta d$ is the change in micrometer reading and $c$ is the sonic velocity in Hg at room temperature and 1 atm . After application and release of pressure, the transit time is found to return to its original value to within 1.4 nsec . In each pressure run half the data points were taken with increasing pressure, and half, with decreasing pressure. Since the delay-line micrometer permits the transit-time change to be determined on the average to about $0.06 \%$ and since the sample length can be measured to about $0.03 \%$, the change in velocity is determined to about $0.09 \%$. The absolute velocity itself, however, is determined to $0.04 \%$, including the

[^3]

Fig. 2. The sample holder for liquid Hg (dimensions in inches).
uncertainty of the 1 -atm data of Hubbard and Loomis, since the velocity change is only a fraction of the calculated velocity.

The sample holder for the liquid Hg , shown in Fig. 2, was constructed from Type 303 stainless stecl. It is closed at the bottom by the quartz transducer and fitted at the top with a $1.2-\mathrm{cm}$-diam reflector set accurately parallel to the transducer. Holes in the reflector top allow the pressure-transmission fluid (pentane or hexane) to bear on the Hg. A final cap, which contains small holes out of line with those in the reflector top, is threaded into the reflector top. This cap acts as a baffle for preventing Hg from escaping from the top of the holder. Loss of mercury into the steel pressure vessel often results in an embrittlement of the latter and an explosive failure.

The diameter of the transducer surface in contact with the liquid $\mathrm{Hg}(1.9 \mathrm{~cm})$ constitutes the sample diameter. Since the wavelength of $5-\mathrm{Mc} / \mathrm{sec}$ ultrasonic waves in liquid Hg is about 0.03 cm , the sample-diameter-to-wavelength ratio is about 00 , well above the figure of 20 which Mason ${ }^{29}$ cites as the minimum allowable value if the sound pulses are to be propagated as if the sample were infinite. The sample length over Which the sound pulse radiates as a plane wave (the Fresnel region) is determined by the diameter of the radiating surface and the wavelength of the sound. ${ }^{30}$ In the present case, where the reflector diameter is the limiting diameter, it can be shown that the Fresnel region extends for 22 cm . Therefore, the echo of importance here (the first echo), which travels a distance of about 7.8 cm , is well within the plane-wave region.
The high-pressure system used in this work is the piston-and-cylinder apparatus shown in Fig. 3. The vessel is of three-piece construction. The inner cylinder is forced into the middle cylinder under a load of about 400 tons, placing the inner cylinder in compression. The outer cylinder is a soft-iron-pipe safety ring. This

[^4]vessel is capable of containing about 30 kbar pressurc. The top of the vessel is sealed by a standard Bridgman seal. Load is applied to the piston from a 400 -ton hydraulic ram. The bottom of the vessel is sealed by a tapered plug through which the necessary electrical leads are brought. Sheathed leads are sealed into a steel plug with epoxy cement. ${ }^{31}$ The ability of this type of plug to retain the electrical leads at high pressure depends in part on the radial force developed as the plug is forced into the taper at the bottom of the pressure vessel. Consequently, the clearance allowed at the bottom of the pluy is critical; excessive support of the plug will result in blowout of the leads. A disadvantage of this type of plug design is that it is sometimes difficult to control the quality of the plugs, with the result that a sheath may be ejected.

Sonic-velocity experiments were carried out at $21.9^{\circ}$, $40.5^{\circ}$, and $52.9^{\circ} \mathrm{C}$. For the higher-temperature experiments the entire pressure vessel was heated. Temperature inside the vessel was determined by a ChromelAlumel thermocouple brought through the tapered bottom plug; its calibration was traccable to a platinum resistance thermometer. At pressures up to 13 kbar the calibration of a Chromel-Alumel thermocouple changes by negligible amount. ${ }^{32}$ A temperature gradient of less than $0.3^{\circ} \mathrm{C}$ existed across the sample at the higher temperatures; this gradient was found to be insensitive to pressure. The probable error in the stated temperature is about $\pm 0.25^{\circ} \mathrm{C}$.


Fig. 3. The pressure vessel (dimensions in inches).

[^5]Pressure was measured with a wire resistance gauge. Such a gauge must be calibrated against a primary pressure standard or against pressure-fixed points, such as phase-transition pressures, which have been themselves accurately established relative to a primary standard. In this work the gauge was a loosely wound coil of 0.005 -in.-diam Au-2.1\% Cr alloy of about $13-\Omega$ resistance. The details of the gauge preparation and calibration against a precision frec-piston gauge have been given elsewhere. ${ }^{33}$ The gauge resistance is determined with the aid of a six-dial potentiometer to an accuracy of 5 ppm , which means that it was possible to detect a pressure change on the order of 6 bar. The calibration of the gauge is given in Table I. The coefficients given there were obtained by a quadratic leastsquares fit of the gauge-resistance-vs-pressure data. The standard deviation of the data from the leastsquares curve was $0.00008 \Omega$ in approximately $12 \Omega$, which is equivalent to 6 bar.

There is some difficulty with drift in the calibration of Au-Cr pressure gauges. A check on the gauge calibration at $21.9^{\circ} \mathrm{C}$ at the time of the velocity experiments showed that it had drifted by an approximately

Table I. Coefficients of the pressure gauge calibration curve, $\Delta R / R_{0}=A P+B P^{2}$.

| Tempcrature <br> $\left({ }^{\circ} \mathrm{C}\right)$ | $A$ <br> $\left(\mathrm{bar}^{-1} \times 10^{-6}\right)$ | $B$ <br> $\left(\mathrm{bar}^{-2} \times 10^{-13}\right)$ |
| :---: | :---: | :---: |
| 21.9 | 1.070 | -4.7 |
| 40.5 | 1.057 | -7.4 |
| 52.9 | 1.044 | -6.2 |

linear factor of $0.4 \% \pm 0.2 \%$ over the eight-month period between the free-piston-gauge calibration and the velocity experiments in such a way as to make the relative change of resistance smaller for a given change of pressure. Since it would have been prohibitively difficult and expensive to check the calibration at the other two temperatures, it is assumed that the calibration drifted in the same way for those temperatures. The calibration in Table I represents the corrected calibration and is therefore reliable to about $0.4 \%$.

## RESULTS

For the purpose of calculation, the measured pressure dependence of the sound velocity given in Table II is fitted to the equations

$$
\begin{align*}
& P=A+B c_{T}+D c_{T^{2}}^{2}  \tag{1}\\
& c_{T}=A^{\prime}+B^{\prime} P+D^{\prime} P^{2} \tag{2}
\end{align*}
$$

where $P$ is pressure and $c_{T}$ is sonic velocity at temperature $T$. Equation (1) is found to give a better fit at each $T$ since the standard deviation in each case is

[^6]| $T=21.9^{\circ} \mathrm{C}$ |  | $T=40.5^{\circ} \mathrm{C}$ |  | $T=42.9{ }^{\circ} \mathrm{C}$ |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
| Pressure | Velocity | Pressure | Velocity | Pressure | Velocity |
| 1 | 1450.1 | 1 | 1441.5 | 1 | 1435.8 |
| 299 | 1457 | 516 | 1453 | 464 | 1447 |
| 584 | 1463 | 932 | 1463 | 925 | 1457 |
| 989 | 1472 | 1458 | 1474 | 1485 | 1469 |
| 1276 | 1478 | 1930 | 1484 | 1942 | 1478 |
| 1532 | 1483 | 2144 | 1488 | 2511 | 1490 |
| 2106 | 1495 | 2769 | 1500 | 2537 | 1491 |
| 3254 | 1517 | 3080 | 1507 | 3019 | 1500 |
| 3264 | 1518 | 3893 | 1522 | 4232 | 1524 |
| 3490 | 1522 | 4298 | 1530 | 4548 | 1530 |
| 4565 | 1542 | 4483 | 1533 | 4942 | 1537 |
| 5772 | 1564 | 5539 | 1552 | 5470 | 1546 |
| 5907 | 1566 | 5642 | 1555 | 6885 | 1572 |
| 6138 | 1570 | 6518 | 1569 | 6915 | 1573 |
| 7542 | 1594 | 7168 | 1581 | 7746 | 1587 |
| 8310 | 1606 | 7175 | 1581 | 8255 | 1595 |
| 8858 | 1615 | 8309 | 1599 | 9533 | 1616 |
| 8950 | 1616 | 8538 | 1604 | 9954 | 1623 |
| 9894 | 1632 | 9399 | 1618 | 10939 | 1639 |
| 10695 | 1644 | 10318 | 1632 | 11203 | 1642 |
| 10926 | 1648 | 10384 | 1634 | 11503 | 1647 |
| 11485 | 1656 | 11830 | 1656 | 11792 | 1651 |
| 11532 | 1657 | 11922 | 1657 | 12968 | 1669 |
| 11985 | 1664 | 12315 | 1663 | 13023 | 1670 |
| 12035 | 1665 | 13270 | 1677 | 13332 | 1675 |
|  |  | 13709 | 1684 |  |  |
|  |  | 14213 | 1691 |  |  |
|  |  | 14695 | 1698 |  |  |
|  |  | 14921 | 1701 |  |  |

${ }^{\text {a }}$ Pressure in bars, velocity in meters per second.
about a factor of 3 smaller than for Eq. (2). Equation (1) presents a more reasonable picture physically since it predicts a steady increase of velocity with pressure while Eq. (2) predicts a maximum in $c_{T}$ with pressure and a subsequent decrease. The standard deviations from the least-squares curve of Eq. (1) for the three experimental temperatures are shown in Table III along with the coefficients of the curves. The solid curves in Fig. 4 represent the least-squares equations.
It is possible to use the sound-velocity data described above, in conjunction with certain other data, to calculate the specific volume of Hg as a function of $T$ and $P$. The calculation starts with the relation between the sound velocity and adiabatic compressibility

$$
\begin{equation*}
\beta_{\mathrm{ad}}=1 / \rho c_{r^{2}}{ }^{2} \tag{3}
\end{equation*}
$$

and the relation

$$
\begin{equation*}
\beta_{T}=\beta_{\mathrm{ad}}+\left(T \alpha^{2} / \rho C_{P}\right), \tag{4}
\end{equation*}
$$

where $\beta_{T}$ is isothermal compressibility at temperature $T$,
Table III. Least-squares coefficients of the curve $P=A+$ $B c_{T}+D c_{T}{ }^{2}$ and the standard deviation $(\sigma)$ of the velocity data.

| Temperature $\left({ }^{\circ} \mathrm{C}\right)$ | $21.9^{\circ}$ | $40.5^{\circ}$ | $52.9^{\circ}$ |
| :--- | :---: | :---: | :---: |
| $A\left(\right.$ bar $\left.\times 10^{5}\right)$ | 4.1489 | 3.9067 | 4.0715 |
| $B\left(\right.$ bar per $\left.\mathrm{m} / \mathrm{sec}^{\circ} \times 10^{2}\right)$ | -1.025 | -0.9885 | -1.006 |
| $C\left(\right.$ bar per $\left.\mathrm{m}^{2} / \mathrm{sec}^{2} \times 10^{-2}\right)$ | 5.096 | 4.976 | 5.034 |
| $\sigma(\mathrm{~m} / \mathrm{sec})$ | 0.2 | 0.3 | 0.3 |



Fig. 4. The sonic velocity $c_{T}$ in liquid Hg as a function of pressure at several temperatures.
$T$ is absolute temperature, $\alpha$ is volume thermal-expansion coefficient, $\rho$ is density, and $C_{P}$ is specific heat at constant pressure. Since

$$
\begin{equation*}
\beta_{T}=-(1 / V)(\partial V / \partial P)_{T}=(1 / \rho)(\partial \rho / \partial P)_{T} \tag{5}
\end{equation*}
$$

where $V$ is volume, it follows from Eq. (3) that

$$
\begin{equation*}
(\partial \rho / \partial P)_{T}=\left(1 / c_{T}^{2}\right)+\left(T \alpha^{2} / C_{P}\right) . \tag{6}
\end{equation*}
$$

Therefore, on integration with respect to $P$,

$$
\begin{equation*}
\rho_{P, T}=\rho_{o, T}+\int_{1}^{P} \frac{1}{C_{T}^{2}} d P+T \int_{1}^{P} \frac{\alpha^{2}}{C_{P}} d P \tag{7}
\end{equation*}
$$

where $\rho_{0, T}$ is density at 1 atm and $T$, and $\rho_{P, T}$ is density at $P$ and $T$. Evaluation of the two integrals over a range of $T$ yields $\rho$ as a function of $P$ and $T$. The integral of $1 / c_{T}{ }^{2}$ at a given temperature can be evaluated directly from the least-squares velocity curves, using numerical integration, under the assumption that $1 / \mathrm{Cr}^{2}$ varies linearly for small $\Delta P=P_{2}-P_{1}$. To evaluate the second integral, two additional relations can be used, viz.,

$$
\begin{equation*}
\left(\partial \alpha / \partial_{P}\right)_{T}=-\left(\partial \beta_{T} / \partial T\right)_{P} \tag{8}
\end{equation*}
$$

and

$$
\begin{equation*}
\left(\partial C_{P} / \partial P\right)_{T}=-(T / \rho)\left[(\partial \alpha / \partial T)_{P}+\alpha^{2}\right] . \tag{9}
\end{equation*}
$$

If $\beta_{T}$ is known as a function of $T$ at $P=P_{1}$, the initial slope of the $\alpha$-vs- $P$ curve may be determined for any temperature. Then, over the interval $\Delta P=P_{2}-P_{1}$, the change of $\alpha$ can be approximated by
$\alpha_{P}=\left(\partial \alpha / \partial_{P}\right)_{T, P_{1}}\left(P-P_{1}\right)+\alpha_{P_{1}}, \quad P_{1} \leq P \leq P_{2}$.
If $\alpha$ vs $T$ is known at $P_{1}, \alpha$ vs $T$ at $P_{2}$ may be found from (10). Therefore, in (9), $(\partial \alpha / \partial T)_{P}$ can be expressed as
$\left(\frac{\partial \alpha}{\partial T}\right)_{P}=\left[\frac{(\partial \alpha / \partial T)_{P_{2}}-(\partial \alpha / \partial T)_{P_{1}}}{\Delta P}\right]\left(P-P_{1}\right)+\left(\frac{\partial \alpha}{\partial T}\right)_{P_{1}}$,

$$
\begin{equation*}
P_{1} \leq P \leq P_{2} \tag{11}
\end{equation*}
$$

Using (11) and the square of (10), Eq. (9) may be integrated analytically to find $\Delta C_{P}$ if $\rho$ is assumed constant over $\Delta P$. This produces a negligible error if $\Delta P$ is small. On performing the integration, $\Delta C_{P}$ is found to be very small so that $C_{P}$ may be assumed constant for the integration in (7). Only the integral of $\alpha^{2}$ at each temperature needs then to be evaluated. This can be found by using the square of (10) and integrating analytically. The density at $P_{2}, \rho_{P_{2}, T}$ is therefore determined.

It is apparent that in the course of calculating $\rho_{P_{2}, T}$ both $C_{P}$ and $\alpha$ have been determined as a function of $T$ at $P_{2}$. Clearly, then, $\beta_{T}$ may be calculated as a function of $T$ at $P_{2}$ from Eq. (4). It follows that the calculation may be now repeated starting with the integration of $1 / c_{T^{2}}$ over the interval $\Delta P=P_{3}-P_{2}$ and the determination of $(\partial \alpha / \partial T)_{P}$ at $P_{2}$ from Eq. (8). By continual repetition of these calculations all the quantities $\beta_{T}, \alpha, C_{P}, \rho$, and $\beta_{\text {ad }}$ may be determined as a function of temperature and pressure. In the experiments described above the change of velocity with

Table IV. One-atmosphere input data to the compression calculation.

| Temperature, $t\left({ }^{\circ} \mathrm{C}\right)$ | $21.9^{\circ}$ | $40.5^{\circ}$ | $52.9^{\circ}$ |
| :--- | ---: | ---: | ---: |
| Density, $\rho\left(\mathrm{g} / \mathrm{cm}^{3}\right)^{\mathrm{a}}$ | 13.54122 | 13.49573 | 13.46551 |
| Thermal-expansion <br> coefficient, $\alpha$ <br> $\left({ }^{\circ} \mathrm{C}^{-1} \times 10^{4}\right)^{\mathrm{b}}$ | 1.81069 | 1.80825 | 1.80699 |
| Specific heat, $C_{P}$ <br> $\left(\text { (ergs } / \mathrm{g} \cdot \mathrm{deg}^{\circ} \times 10^{-6}\right)^{\mathrm{c}}$ | 1.390 | 1.385 | 1.382 |
| Sonic velocity $C_{T}$ <br> $(\mathrm{~m} / \mathrm{sec})^{\mathrm{d}}$ | 1450.1 | 1441.5 | 1435.8 |

${ }^{\text {a }}$ Reference 36.
${ }^{5}$ Reference 35.
${ }^{\circ}$ Reference 34.
${ }^{d}$ Reference 27

Table V. Calculated variables.

pressure, for three temperatures, has been established while the change of velocity with temperature at 1 atm is given by Hubbard and Loomis. ${ }^{27}$ The values for $C_{P}$ at 1 atm and various temperatures are given by Douglas ct al. ${ }^{34}$ to an accuracy of $0.3 \%$. Values for $\alpha$ at atmospheric pressure and $T$ have been taken from the work of Beattie et al. ${ }^{35}$ which establishes $\alpha$ within about 1 part in $10^{5}$. The density $\rho$ is given by Bigg, ${ }^{36}$ who used the most recent determination of the density of Hg at

[^7]$20^{\circ} \mathrm{C}$, in conjunction with Beattie's expansion formula, to determine $\rho$ as a function of temperature to within about 4 ppm . Using the data for $\rho$ and the sonicvelocity data of Hubbard and Loomis, the adiabatic compressibility of liquid Hg may be calculated according to Eq. (3). Using $\beta_{\mathrm{ad}}$, and $\alpha$ and $C_{P}$ from the above sources, $\beta_{T}$ may be calculated according to Eq. (4). All the data are thus established for the initiation of the calculation at $P_{1}=1 \mathrm{~atm}$. The numerical values of the input data are shown in Table IV.

The results of the calculation for $\alpha, \beta_{T}, \beta_{\mathrm{ad}}, \rho$, and $V$ as a function of $P$ at $21.9^{\circ}, 40.5^{\circ}$, and $52.9^{\circ} \mathrm{C}$ are shown in Table V. Figures 5-7 show the variation of $\alpha, \beta_{T}$, and $V$ with pressure. No variation of $C_{P}$ with $P$


Fig. 5. The volume thermal-expansion coefficient $\alpha$ of liquid Hg vs pressure at several temperatures. Considering experimental error, the three curves are actually just barely distinguishable from one another.
greater than experimental error is detected, hence its calculated variation with pressure has not been shown in a table or graph.
The procedure adopted here for estimating the probable error associated with each of the calculated results is to place various perturbations on the input data for the calculation and to observe its effect on the results. Since the three major sources of uncertainty in the present work are the results of the experimental determination of sonic velocity as a function of pressure, the $1-\mathrm{atm}$ velocity data of Hubbard and Loomis, and the $C_{P}$ data of Douglas et al., three perturbations, each involving only one of these variables, are investigated. The uncertainties in $\alpha$ and $\rho$ at atmospheric pressure and in the temperature are negligible in comparison. The errors in $\beta_{T}$ and $\beta_{a d}$ at atmospheric pressure are taken into account automatically by considering the three major uncertainties.
To account for the errors in the velocity experiments, all the uncertainty may be assumed, for convenience, to be in the pressure scale. The possible systematic error in the scale itself is of the order of $0.4 \%$. To this must be added a measure of the random uncertainty as indicated by the standard deviation $\sigma$ of the velocity data from the least-squares curves. The equivalent of this $\sigma$ on the pressure scale is about 17 bars. This uncertainty varies in percentage over the pressure scale, but a reasonable average is $0.3 \%$. The total uncertainty on the pressure scale is therefore about $0.7 \%$. In accordance with this, the least-squares velocity curve at $21.9^{\circ} \mathrm{C}$
was adjusted so that a given velocity would correspond to a pressure higher than the experimentally determined value by $0.7 \%$, and the $52.9^{\circ}$ data was adjusted to predict a pressure lower by $0.7 \%$. This adjustment may be made by multiplying the coofficients of the least-squares curves by an appropriate constant. The curve at $40.5^{\circ} \mathrm{C}$ was unadjusted. This perturbation can also be viewed as an adjustment of the slope of $c_{T}$ vs $T$ at each pressure. Since the perturbation involves a change of slope rather than a uniform increase or decrease of the data, it will affect the results for the three temperatures differently at a given pressure. Choosing the maximum effect should give a reliable estimate of the largest likely error.

The effects on $\alpha, \beta_{T}, V$, and $C_{P}$ of performing the calculation with the perturbation on the pressure scale are shown in Table VI. They are shown only for 13 kbar for the sake of brevity. To a first approximation the effect of the perturbation on each quantity decreases linearly, with decreasing pressure, to its value at 1 atm . Since the calculated change in $C_{P}$ for each temperature was about $0.25 \%$ at 13 kbar , it follows, according to the effect of the perturbation on $C_{P}$ (about $\pm 0.75 \%$ ), that no information can be gained from the present work regarding the sign of change or rate of change of $C_{P}$ with pressure.
The second perturbation on the data was constructed by reducing the value of $C_{P}$ at 1 atm and $21.9^{\circ} \mathrm{C}$ by $0.3 \%$ and by raising it $0.3 \%$ at $52.9^{\circ}$. The third perturbation was obtained by decreasing the sonic velocity at $21.9^{\circ}$ and 1 atm by $0.02 \%$ and by raising it at $52.9^{\circ} \mathrm{C}$ by the same percentage. The effects on $\alpha, C_{P}, \beta_{T}$, and $V$ of carrying out the calculations with these perturbations are also shown in Table VI. An estimate of the uncertainty of each quantity is then obtained by taking the sum of the perturbation effects, and it amounts to $\pm 0.4 \%$ for $\beta_{T}, \pm 1.0 \%$ for $\alpha, \pm 1.3 \%$ for $C_{P}$, and $\pm 0.0094 \%$ for $V$. Once again, to a first approximation,


Fic. 6. The isothermal compressibility $\beta_{T}$ of liquid Hg as a function of pressure at several temperatures.

Fic. 7. The relative volume $V$ of liquid Hg as a function of pressure at several temperatures. Volume at 1 atm and

the uncertainty in each quantity decreases linearly with decreasing pressure to its value at 1 atm . These have been listed previously, except for $\beta_{T}$, for which it is $0.8 \%$.

Selection of the appropriate value of the interval $\Delta P$ to be used in the calculation of the thermodynamic variables is a matter of trial and error. It was found that there was no need to use an interval smaller than 125 bar. The residual error for each variable which results from using this interval is between one and two orders of magnitude smaller than the uncertainty of the variable.

The thermodynamic calculations which have been described were programmed for an IBM 1620 computer. In order to compute the derivatives $(\partial \beta / \partial T)_{P}$ and $(\partial \alpha / \partial T)_{P}$ of Eqs. (8) and (9), respectively, it was necessary to fit curves by the least-squares method to the $\beta_{T}$-vs- $T$ and $\alpha$-vs- $T$ data at each step of pressure. Curves of the type

$$
\begin{equation*}
\beta_{T}=A+B T+G T^{2} \tag{12}
\end{equation*}
$$

and

$$
\begin{equation*}
\alpha=D+E T+F T^{2} \tag{13}
\end{equation*}
$$

are chosen since they accurately describe the variation at 1 atm of $\beta_{T}$ and $\alpha$ with $T$ over the range of $0^{\circ}-100^{\circ} \mathrm{C}$. The suitability of these equations for fitting the temperature data at higher pressures can be easily checked as the calculation proceeds, and, if necessary, different equations could be used over different intervals of pressure. In the present work the use of a quadratic in $T$ leads to a perfect fit since there are only three data points with temperature variation; since the data display a definite curvature, use of a straight line would not be suitable.

Each of the three perturbations described above left the data at $40.5^{\circ} \mathrm{C}$ unperturbed, while the data at $21.9^{\circ}$ and $52.9^{\circ}$ were adjusted in opposite directions. The perturbations were purposely chosen this way to maximize the variation in the derivatives $(\partial \beta / \partial T)_{P}$ and $(\partial \alpha / \partial T)_{P}$ and thus establish the maximum likely un-
certainty in the calculated results. The largest uncertainties occur in $\alpha$ and $C_{P}$ because of their strong dependence on these derivatives through Eqs. (8) and (9), respectively. The uncertainty in $\beta_{T}$ is smaller because the uncertainties of $\alpha$ and $C_{P}$ affect it only through the additive term in Eq. (4) $T \alpha^{2} / \rho C_{P}$, which is about $10 \%$ of $\beta_{T}$. The volume is obtained with high accuracy because it involves the uncertainties in the velocity data and $\alpha$ and $C_{P}$ through the small additive integrals in Eq. (7). The accuracy of $\beta_{\text {ad }}$ is affected mainly by the uncertainty in the sonic velocity since the volume is quite accurate, and thus it is accurate to about $0.14 \%$.

## DISCUSSION

High accuracy in pressure measurement can only be attained below about 13 kbar where calibration against free-piston gauges is possible. The possibility that more precise volume data at very high pressure may be obtained by appropriate extrapolation of relatively precise data taken below 13 kbar than by direct measurement has been pointed out by Anderson. ${ }^{37}$ For this reason it is of interest to consider the question of the best analytical representation of experimental $P-V$ data. The precision volume results for Hg provide an

Table VI. Magnitude of the perturbation effects on the calculated variables at $13 \mathrm{kbar}{ }^{\text {a }}$

| Variable | $\beta_{T}$ | $\alpha$ | $C_{P}$ | $V$ |
| :--- | :---: | :---: | :---: | :---: |
| $C_{P}$ perturbation | 0.07 | 0.2 | 0.30 | 0.0019 |
| Pressure scale perturba- <br> tion | 0.26 | 0.6 | 0.75 | 0.0057 |
| One-atmosphere velocity <br> perturbation <br> Total | 0.07 | 0.2 | $\frac{0.25}{1.0}$ | $\underline{1.3}$ |

${ }^{\text {a }}$ In percent.
${ }^{37}$ O. L. Anderson, J. Phys. Chem. Solids 27, 547 (1966).


Fig. 8. The deviations of the volume data from the least-squares fitted equations of state. Limits of experimental error indicated by sloping straight lines.
opportunity for testing the usefulness of various isothermal $P-V$ equations.

To be uscful in the representation of $P-V$ data for a given phase, an equation must be single valued and continuous for all pressures, $V$ must be greater than zero but decrease for all $P$, and $d V / d P$ must decrease continuously. These conditions suppose no phase changes under pressure; if phase changes occur, the extrapolation method is no longer useful. Of equations satisfying the above conditions, the most satisfactory will be that which can best fit existing data with the smallest number of fitting coefficients. A further desirable property is that the coefficients be directly related to some physical property of the material considered.

A direct approach to developing a $P-V$ equation would be to express the Helmholtz free energy as a power series in $V$ and use the relation $P=-(\partial F / \partial V)_{T}$. An equivalent, and easier, method is to use a Taylor series expansion of the pressure in terms of the volume. The expression for $F$ then follows from integration of $P$ with respect to $V$.

Considering the conditions listed above for a pres-sure-volume equation, a likely choice is to expand the pressure in powers of $V_{o} / V$, about $V_{o} / V=1$ or $V=V_{o}$. This expression, up to the quadratic term, is

$$
\begin{align*}
P=\frac{d P}{d\left(V_{o} / V\right)_{V=V_{0}}} & \left(\frac{V_{0}}{V}-1\right) \\
& +\frac{1}{2} \frac{d^{2} P}{d\left(V_{o} / V\right)^{2} V=V_{0}}\left(\frac{V_{o}}{V}-1\right)^{2}+\cdots, \tag{14}
\end{align*}
$$

where $V_{0}$ is initial volume. The cocfficients of the expansion can be written as

$$
\frac{d P}{d\left(V_{0} / V\right)_{V-V_{0}}}=B_{0}
$$

and

$$
\frac{d^{2} P}{d\left(V_{0} / V\right)_{V=V_{0}}}=B_{0}\left(B_{0}^{\prime}-1\right),
$$

where $B_{0}$ is the bulk modulus at 1 atm and $B_{o}{ }^{\prime}$ is the derivative of the bulk modulus with respect to pressure, evaluated at 1 atm . Equation (14) can be expressed, therefore, as

$$
\begin{equation*}
P=B_{o}(\Delta V / V)+\frac{1}{2} B_{o}\left(B_{o}^{\prime}-1\right)(\Delta V / V)^{2}+\cdots \tag{15}
\end{equation*}
$$

where $\Delta V=\left(V_{0}-V\right)$. This equation meets the requirements listed above since it is single valued and continuous, and it predicts a volume which steadily decreases at a decreasing rate with increasing pressure but always remains real and positive, provided that $B_{o}{ }^{\prime}$ is greater than 1 .

A related but alternate approach has been suggested by Onat ${ }^{38}$ and by Vaisnys ${ }^{39}$ whereby the pressure is expanded in powers of $\ln V$ about $V=V_{o}$ :

$$
\begin{align*}
P=(d & P / d \ln V)_{V=V_{0}}\left(\ln V-\ln V_{0}\right) \\
& +\frac{1}{2}\left(d^{2} P / d \ln V^{2}\right)_{V=V_{0}}\left(\ln V-\ln V_{0}\right)^{2}+\cdots \tag{16}
\end{align*}
$$

Again, the coefficients may be expressed in terms of $B_{0}$ and $B_{o}{ }^{\prime}$, viz.,

$$
(d P / d \ln V)_{V=V_{0}}=-B_{o}
$$

and

$$
\left(d^{2} P / d \ln V^{2}\right)_{V=V_{0}}=B_{0} B_{0}^{\prime},
$$

so that Eq. (16) may be written as

$$
\begin{equation*}
P=-B_{0} \ln \left(V / V_{o}\right)+\frac{1}{2} B_{o} B_{o}^{\prime}\left[\ln \left(V / V_{o}\right)\right]^{2}+\cdots \tag{17}
\end{equation*}
$$

This equation also meets the requirements listed above.
A number of other equations to describe the pressurevolume relations of materials have been proposed by various investigators. Bridgman expressed a great deal

[^8]of his compression data with a Taylor-scrics expansion of $V$ in powers of $P$ about $P=0$ (the rest he put in tabular form):
\[

$$
\begin{equation*}
V=V_{0}+(d V / d P)_{P=0} P+\frac{1}{2}\left(d^{2} V / d P^{2}\right)_{P=0} P^{2}, \tag{18}
\end{equation*}
$$

\]

where
and

$$
(d V / d P)_{P=0}=-V_{0} / B_{0}
$$

$$
\left(d^{2} V / d P^{2}\right)_{P=0}=V_{0}\left(1+B_{0}{ }^{\prime}\right) / B_{0}{ }^{2} .
$$

Ife found that, within the accuracy of his data, this cquation gave a good representation of the compression of many substances. Recently Anderson and Schreiberi0 have determined the values of $B_{0}, B_{0}{ }^{\prime}$, and $B_{0}{ }^{\prime \prime}$, where $B_{o}{ }^{\prime \prime}$ is the second derivative of the bulk modulus evaluated at 1 atm , for polycrystalline magnesium oxide. They uscd this data in conjunction with Eq. (18), expanded to include the additional terms in $P^{3}$ and $P^{4}$, to express the equation of state of MgO . Examination of this type of expansion, however, shows that it does not meet all the stipulations required for a satisfactory $P-V$ relation. Since the coefficients of all the odd powers of $P$ will be negative and the coefficients of all the even powers will be positive, the expansion predicts that the volume will approach negative infinity, with increasing pressure, if it is cut off at an odd power of $P$ and that it will approach positive infinity when the last term involves an even power of $P$. In the latter case the volume will also be a double-valued function of the pressure.
In another approach to a $P-V$ equation, Murnaghan ${ }^{41}$ has suggested expanding the bulk modulus as a function


Fig. 9. The isothermal bulk modulus $B$ of liquid Hg vs pressure at several temperatures.

[^9]| $P$ (kbar) | $T\left({ }^{\circ} \mathrm{C}\right)$ |  |  |
| :---: | :---: | :---: | :---: |
|  | $21.9^{\circ}$ | $40.5^{\circ}$ | $52.9{ }^{\circ}$ |
| 0 | 248.4 | 243.1 | 239.6 |
| 1 | 257.6 | 252.4 | 248.9 |
| 2 | 266.6 | 261.3 | 257.9 |
| 3 | 275.3 | 270.1 | 266.7 |
| 4 | 284.0 | 278.7 | 275.4 |
| 5 | 292.5 | 287.3 | 283.9 |
| 6 | 300.8 | 295.6 | 292.3 |
| 7 | 309.1 | 303.9 | 300.5 |
| 8 | 317 | 312 | 309 |
| 9 | 325 | 320 | 317 |
| 10 | 333 | 328 | 325 |
| 11 | 341 | 336 | 333 |
| 12 | $349$ | 344 | 341 |
| 13 | 357 | 352 | 348 |

${ }^{a}$ Units of kilobars.
of $P$, according to the relation

$$
\begin{equation*}
B=-V(d P / d V)=B_{0}+B_{o}^{\prime} P . \tag{19}
\end{equation*}
$$

On integration this gives the so-called "Murnaghan logarithmic equation,"

$$
\begin{equation*}
\ln \left(V_{0} / V\right)=\left(1 / B_{0}^{\prime}\right)\left\{\ln \left[\left(B_{0}+B_{0}^{\prime} P\right) / B_{0}\right]\right\}, \tag{20}
\end{equation*}
$$

which satisfies the listed requirements. Equation (19) can be expanded to include terms of higher power in the pressure, but this may lead to peculiarities in the resulting pressure-volume expression: If the bulk modulus expression is expanded, for example, to include $B_{o}{ }^{\prime \prime}$ and this coefficient is negative, the bulk modulus will eventually pass through a maximum with pressure and then become negative. Birch ${ }^{42,43}$ has used Murnaghan's ${ }^{44}$ theory of finite strain and a series expansion of $F$ in terms of $V$ to derive the equation

$$
\begin{equation*}
P=\frac{3}{2} B_{0}\left[\left(V_{0} / V\right)^{7 / 3}-\left(V_{0} / V\right)^{5 / 3}\right]\left\{1-\xi\left[\left(V_{0} / V\right)^{2 / 3}-1\right]\right\}, \tag{21}
\end{equation*}
$$

where

$$
\xi=\frac{3}{4}\left(4-B_{o}^{\prime}\right) .
$$

Since the definition of strain (for strains larger than infinitesimal) is arbitrary, this equation has no particularly unique relation to elasticity theory. It does meet the requirements for an equation of state listed at the beginning of this section, provided $B_{0}{ }^{\prime}$ is greater than 4.

Each of the equations enumerated above has been tried against the Hg volume data. $B_{o}$ is fixed at its independently determined value at $P=0$. Each of the equations then has only one adjustable parameter, which may be expressed in terms of $B_{o}^{\prime}$ '; this is chosen to give a minimum standard deviation. The deviations of these equations from the volume data are shown in

[^10]Table VIII. Standard deviation ( $\sigma$ ) for the equations of state (in terms of $V / V_{0}$ ) and the pressure derivative of the bulk modulus ( $B_{0}{ }^{\prime}$ ).

| Equation | $21.9^{\circ} \mathrm{C}$ | $40.5^{\circ} \mathrm{C}$ | $52.9^{\circ} \mathrm{C}$ |  |
| :---: | :---: | :---: | :---: | :---: |
| $\sigma($ unitless $)$ |  |  |  |  |
| Quadratic $\left(V / V_{0}=1+a P+b P^{2}\right)$ | $235 \times 10^{-6}$ | 250 | 260 |  |
| Cubic $\left(V / V_{0}=1+a P+b P^{2}+c P^{3}\right)$ | 18 | 20 | 21 |  |
| Murnaghan's cquation $(20)$ | 38 | 40 | 42 |  |
| Birch's cquation (21) | 10 | 11 | 12 |  |
| $(17)$ | 29 | 31 | 32 |  |
| .$(15)$ | 8 | 9 | 9 |  |
|  |  | $B_{0}{ }^{\prime}$ (unitless) |  |  |
| Murnaghan's cquation (20) | 8.70 | 8.72 | 8.74 |  |
| Birch's cquation (21) | 9.10 | 9.14 | 9.17 |  |
| $(17)$ | 9.72 | 9.78 | 9.81 |  |
| $(15)$ | 9.38 | 9.44 | 9.47 |  |

Fig. 8. This figure specifically pertains to the volume data at $21.9^{\circ} \mathrm{C}$, but the results at $40.5^{\circ}$ and $52.9^{\circ} \mathrm{C}$ are almost identical. The straight lines shown at an angle to the zero deviation line represent the probable limits of error of the volume data less any systematic error in the pressure scale since this would not influence the fit of the various equations tested. It has already been indicated that, on general grounds, Eq. (18) is a poor choice as an equation of state, but in addition, as Fig. 8 shows, it gives a very poor fit to the present data. The cubic expansion of $V$ in terms of $P\left(\Delta V / V_{o}=\right.$ $a P+b P^{2}+C P^{3}$ ) was also fitted and found not to give a very good representation of the data, and of course the equation begins to diverge strongly toward negative infinity at pressures slightly above the experimental range. Equations (15) and (21) each represent the data with the use of only one adjustable parameter; each predicts a reasonable extrapolation of the volume to higher pressures. Murnaghan's logarithmic equation (20) and Eq. (17) do not provide an adequate representation of the volume change with pressure. In the case of Murnaghan's equation, this indicates that the bulk modulus of Hg does not vary linearly with $P$ to 13 kbar. Figure 9 shows that the bulk modulus $B$ does indeed deviate slightly from linearity with pressure. By obtaining a least-squares fit of a straight line $\left(B_{0}+B_{o}{ }^{\prime} P\right)$ to the bulk-modulus data and noting the deviations of the data from this line, it was confirmed that the curvature of $B$ is outside experimental error. The bulk-modulus data is also shown in Table VII.

Table VIII lists the standard deviations of the equations tested and also $B_{o}^{\prime}$ for Murnaghan's equation,
for Eq. (17), and for the two equations which best represent the data.

In summary, it is seen that two equations give a good fit to the volume data: Eq. (15), an expansion of $P$ in terms of $V_{o} / V$, and the Birch equation (21). The Murnaghan and Bridgman equations are not satisfactory, and the latter is not suitable for extrapolation. No one of these equations has more theoretical justification than another. Considering its simplicity, Eq. (15) is the most satisfactory analytical representation of the $P-V$ data which satisfies all of the criteria established above. It does not appear to have been used for this purpose before. If a third term were required in this equation, it would be

$$
\frac{1}{6} \frac{d^{3} P}{d\left(V_{o} / V\right)^{3}}=\frac{1}{6}\left[2 B_{o}-3 B_{o}^{\prime} B_{o}+\left(B_{o}\right)^{2} B_{o}+B_{o}^{\prime \prime} B_{0}^{2}\right] .
$$

The method of calculation which has been developed for the analysis of the mercury data can easily be modified to be applicable to isotropic solids. The principal difference is that, whereas the length of the liquid sample is known at all pressures, that of the solid is not. Letting the ratio of the initial length of an isotropic solid sample to the length at pressure $P$ be $S$, i.e.,

$$
\begin{equation*}
S=l_{0} / l=\left(\rho / \rho_{0}\right)^{1 / 3} \tag{22}
\end{equation*}
$$

it can be shown that

$$
\begin{align*}
& S=1+\int_{0}^{P} \frac{1}{4 l_{o}^{2} \rho_{0}\left[3\left(1 / l_{1}\right)^{2}-4\left(1 / t_{2}\right)^{2}\right]} d P \\
& \quad+\frac{T}{3 \rho_{o} S^{2}} \int_{0}^{P} \frac{\alpha^{2}}{C_{P}} d P \tag{23}
\end{align*}
$$

where $t_{1}$ and $t_{2}$ are the transit times for longitudinal and shear wave pulses, respectively. In this case solution of the two integrals gives $S$ and, from Eq. (22), $\rho$ as well as the sonic velocities. The quantity $S$ appears outside of the integral in the second term of Eq. (23); this is correct if the integral is evaluated over a small interval $\Delta P$ within which $S$ may be considered constant, analogous to the procedure used with the liquid.

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